

Assessment of Biogas Potential of Pineapple Waste in Mono and Co- Digestion with Cow Dung at Ambient Temperature

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Abstract

Pineapple (*Ananas comosus* (L.) Meril) processing in Benin's agri-food industries generates waste with high potential for energy production. The present study assessed the biogas production potential of pineapple cakes and crowns in mono and co-digestion with cow dung. The methodology used is based essentially on the Simplex-Centroid Designs mixing scheme designed in Minitab.19. Anaerobic digestion tests were carried out with seven formulations in triplicate. Temperature, pH and biogas volume were monitored. A predictive model of biogas production according to mixing ratios was developed. Results indicate that digesters operating at mesophilic temperatures ranged from 23°C to 33°C, with an average of 26.5°C±0.33. The best-performing mixture in terms of biogas volume generated contained 50 g cake:50 g cow dung. This resulted in the production of 9.62 liters of biogas/kg of waste. Therefore, it has been established that pineapple waste and cow dung can be used efficiently for biogas production. The results also reveal the importance of maintaining some physico-chemical parameters of the waste mixtures in order to optimize biogas production. The model approximates average biogas production, with an R² correlation coefficient over 80%. In total, pineapple waste can be used to produce biogas. The exploitation of this energy resource in agri-food industries can contribute to the use reduction of conventional energy and fossil fuels.



Article History

Received: 14 October 2024

Accepted: 23 December 2024


Keywords

Anaerobic;
Benin; Biogas;
Cow Dung,
Pineapple-Waste.

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Doi: <https://dx.doi.org/10.12944/CWE.20.1.8>

Introduction

The anaerobic digestion of biomass represents a promising approach to mitigate the effects of global warming and combat the greenhouse effect. It offers a sustainable, green, and substitute energy source for non-renewable energy sources, whose supplies are running low at an accelerating rate.¹

A biological process called anaerobic digestion breaks down organic materials into simpler ones to create energy (biogas) and fertilizer (digestate) by a microorganism's actions. Biogas is a combination of gases consisting mainly of methane (40-75%), and carbon dioxide (25-50%), with smaller amounts of additional gases, including hydrogen sulfide (H₂S), ammonia (NH₃), oxygen (O₂), hydrogen (H₂), nitrogen (N₂), and carbon monoxide (CO).²⁻³ Methane contained in biogas is an excellent source of heat and electrical power generation.⁴ The heating value of well-purified biogas is close to that of natural gas.⁵ Anaerobic digestion technology has the advantage of treating main organic waste,⁶ giving biogas a strong potential for sustainability.⁷ Organic waste can be classified as follows: vegetable waste, animal waste, food waste, fruit waste, and agricultural residues.⁸

Pineapple, *Ananas comosus* (L.) Merr., a tropical edible fruit belonging to the Bromeliaceae family, is regarded as a significant fruit because of its accessibility to a large number of people, excellent nutritious content and a delicious taste.^{9,10} In Benin, pineapple is among the most significant fruit varieties, representing the third most valuable export potential after cotton and cashew. In 2019, it contributed 0.42% of the national GDP and 1.95% of the agricultural GDP.¹¹ They come in the varieties known as Smooth Cayenne and Sugarloaf. It is more prone to deterioration since it contains roughly 85% moisture, necessitating manufacturing or instantly consumption.¹² According to estimates, approximately 264,834 tons of raw pineapple were marketed in 2020-2021.¹³ Only around 99,814 tons are processed mainly into juice by all the units counted.¹¹ These quantities undergo processing at three distinct scales: artisanal, semi-industrial, and industrial. The common characteristic of units is to generate a finished product to consume. They coexist in a state of equilibrium, forming a continuum of activities with well-defined characteristics and responding to different market segments.¹⁴

Processing pineapple into juice is very energy-intensive. Most semi-industrial and industrial units use wood, butane gas, conventional electricity, and diesel. However, due to the inflation in energy costs over the last decade, most processing units are encountering significant challenges in procuring supplies.¹⁴ Pineapple manufacturing produces wastes (pulp, peel, core, stem, crown, and leaves) representing 60% (w/w) of the entire weight of the pineapple. These have many unique properties that warrant further investigation.¹² This organic waste is unutilized and continually stored close to the units. Consequently, this accumulation of waste can contribute to (i) the pollution of soil, surface, and groundwater, (ii) the degradation of air quality due to the putrefaction of this waste giving off unpleasant odors and irritating vapors, and (iii) the emission of greenhouse gases into the atmosphere and global warming. Pineapple waste is the usual instance of biomass made of lignocellulosic material with a huge capacity for energy production but is not yet used as a durable, ecological, and clean source.¹⁵ Mamo T *et al.*¹⁶ reported that biogas outputs from pineapple peels range from 0.41- 0.67-meter cube per kilogram (m³/kg) volatile solids with a 41–65% methane concentration.

Biogas productivity of substrates is affected by physico-chemical conditions such as feedstock type, pH, temperature, carbon (C) and nitrogen (N) content, chemical oxygen demand (COD), etc. Anaerobic co-digestion might represent a promising approach for enhancing methane yields.¹ In order to improve the anaerobic digestion process, co-digestion entails treating substrates jointly to give the microorganisms the necessary carbon and nutrients.¹⁷ Although microbial activity can be supported by separate substrates, mixing substrates frequently produces a synergistic effect in which the mixture's methane yield is greater than the sum of its parts. However, depending on the makeup and ratios of the substrates, antagonistic effects, including a decrease in methanogenic activity, can also happen.¹⁸ The potential of codigestion for methane optimisation is demonstrated by studies. Study,¹⁹ for instance, showed that a 1:1 ratio of food waste to fruit and vegetable waste stabilised the digestion process and enhanced methane generation to 0.49 m³ CH₄/kg volatile solids. In a similar vein, study²⁰ found that co-digesting jackfruit waste, pineapple

peels, and banana peels with 25% cow dung increased biogas output by two to three times. By co-digesting tomato pulp with animal dung, study²¹ was able to generate the maximum methane yield, 404 ml CH₄/gVS, underscoring the significance of preserving a higher proportion of animal dung for best outcomes. On the other hand, Sitorus and associates²² found that the high acidity of plant waste may prevent methanogenic activity because of the quick acidification and volatile fatty acid buildup. Notwithstanding these challenges, co-digestion with animal waste stabilises the anaerobic digestion process by providing vital nutrients and buffering capacity.³ This was shown by Mukumba and partners,²³ who discovered that a 75% methane composition was produced by an equal mixture of cow, goat, donkey, and horse excrement.

Any project of residue valorization through anaerobic digestion requires the knowledge of biogas generation potential to provide the technical elements needed for an economic feasibility study. However, this knowledge on pineapple residues remains limited. Several methods exist to determine the biogas or biomethane potential of a given residue or combination of residues. Estimates can be made based on the chemical or biochemical composition of the residue.²⁴ These estimates do not take into account

several factors: inhibition phenomena due to the presence of certain substances or overloading, the biodegradability of the material, the conditions of the reaction medium, and the proportion of the substrate consumed by the microbial flora for its growth.²⁵ Biochemical Methane Production (BMP) test also can be used to evaluate objectively this potential.^{24,26}

This article aims to optimize the production of biogas from pineapple residues. It investigates the biogas production potential of pineapple waste in mono and co-digestion with cow dung at ambient temperature and to determine which organic waste mixture is best suited to biogas production.

Materials and Methods

Research Area

The investigation was conducted in the West African nation of Benin (114.763 km²), which is situated between 06°15' and 12°25' north latitude and 0°40' and 3°45' east longitude. Throughout the country, average annual temperatures vary between 26 and 28°C. The yearly temperature range is minimal in the southern region (5 to 10°C), although it is higher (11 to 13°C) in the north (from latitude 8°N northwards). The estimated population of Benin is 9,983,884 inhabitants.

Table 1: Physico-chemical properties of substrates

Parameters	Crown ²⁸	Cake ²⁹	Cow dung ³⁰
Moisture (%) ^h	83.4 ± 1.8	nd	nd
Dry matter (MS) (%) ^h	16.8 ± 1.8	26	21
Volatile solid (MV) (%) ^s	94.9 ± 0.6	nd	nd
A (% ash) ^s	5.1 ± 0.6	2.8	nd
Total soluble sugar ^s	38.14 ± 4.2	4.8	nd
Cellulose (%) ^s	11.63 ± 0.6	34.9	nd
Hemicellulose (%) ^s	13.32 ± 24	28.2	nd
Lignin (%) ^s	15.03 ± 0.6	2.2	nd
Reducing sugars ^s	5.23 ± 0.1	nd	nd
C	44.05	nd	31
H	5.81	nd	85
N	0.87	nd	1.46
O	49.27	nd	17.46
C/N ratio	50.63	43.3	21.4
pH	nd	5.6	7.5

h: wet basis; s: dry basis

Sampling, Preparation, and Characteristics of Wastes

The substrates used in this research were pineapple cakes (pulp residues and peels), crowns, and cow dung.

Pineapple waste comes from Promo Fruits Bénin, situated in Allada (Benin) in southern Benin, 90 km from the capital. The processing capacity of this company is 21,900 tons per year.¹⁴ The cow dung, used as inoculum, comes from the Saclo's slaughterhouse in Bohicon.

In the laboratory, the waste samples were sorted to remove undesirable matters then individually mixed in a blender to minimise their granulometry and enhance their surface area during the test. Then, the

substrates were diluted with water to a total volume that was twice the volume of the substrates.²⁷ The physico-chemical properties of the waste are shown in table 1.

Biogas Generation Potential Tests

To assess the biogas generation potential of the waste, samples were placed in 500 ml serum bottles, which served as reactors with a gas release valve attached to a screw cap. The tests were conducted in batch mode. The experimental design was defined using Minitab's statistical design software (Minitab.19) based on the Simplex-Centroid Designs method,³¹ which was selected due to its simplicity, time, and material availability. Table 2 presents the composition of the substrates in each reactor.

Table 2: Mixing design experiment matrices

Formulation	Proportion (%)		
	C (<i>crown</i>)	T (<i>Cake</i>)	B (<i>cow dung</i>)
R1	100	0	0
R2	0	100	0
R3	0	0	100
R4	50	50	0
R5	0	50	50
R6	50	0	50
R7	33.33	33.33	33.33

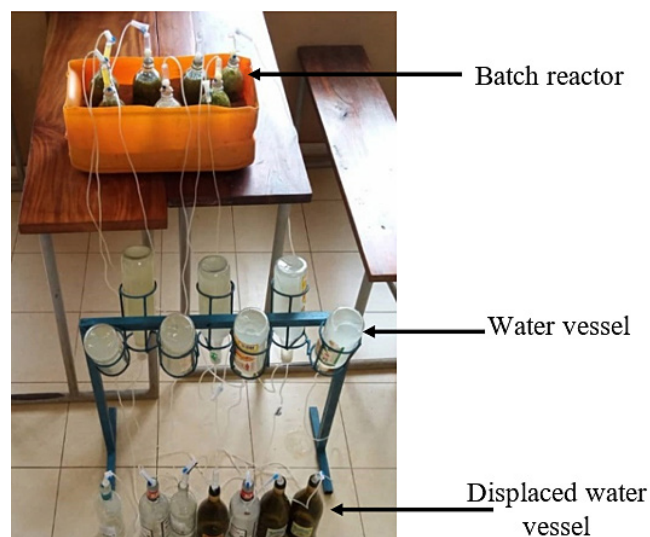


Fig. 1: Experimental design for the anaerobic digestion

All tests were carried out three times, resulting in 21 samples. To maximize the interaction between the substrate and the inoculum, the samples were homogenized. The anaerobic digestion of the substrate was conducted at room temperature according to our experimental design (Figure 2). Each reactor was filled with 100 grams of substrate. The experimental setup is depicted in Figure 1.

The physico-chemical parameters analysed were pH and temperature. The pH of the mixtures was determined weekly using pH paper. Temperature was measured daily using a Benetech laser thermometer. The biogas produced was measured daily using a one-liter bottle calibrated to the nearest millimetre. The downward water displacement method at air pressure for each reactor is used.²⁸ Lemon water was used to prevent the CO₂ in the biogas from being trapped. The amount of water displaced was proportional to the volume of biogas produced. Measurements were taken every day at the same fixed time (01:00 pm). The tests lasted a maximum of 45 days, corresponding to the complete digestion of the last substrate formulation. Each test's cumulative biogas production was calculated by adding together the daily biogas production. Biogas production was monitored and measured until biogas the water level in the bottles stabilised on at least 3 successive days.

Data Processing and Analysis

All experimental data were recorded in Excel spreadsheets. First, the averages were calculated and graphs were created to analyze how the parameters changed over time. Then, biogas production data and mixing factors were used to develop a mathematical simulation model in Minitab 19 using the "Analyze a mixing plan" function. To verify the accuracy of the model, the experimental biogas production values were compared with those obtained from the model. The average difference between the predicted and actual values of the model is measured by the relative residual root mean square error (rRMSE) which is the standardised residual root-mean-square error. The model's ability to predict biogas output is indicated by the coefficient of determination (R²), which ranges from 0 to 1. The closer the model's R² is near 1, the more accurate its predictions will be.

$$RMSE = \sqrt{\frac{1}{N} \sum_{i=1}^N (y_i - \tilde{y}_i)^2} \quad \dots(1)$$

$$rRMSE = \frac{RMSE}{\bar{y}} \quad \dots(2)$$

y_i: measured values

\tilde{y}_i : corresponding adjusted values

\bar{y} : average measured value

N: number of measurements performed

$$R^2 = 1 - \frac{SCR}{STC} \quad \dots(3)$$

With

$$SCR = \sum_{i=1}^N (y_i - \tilde{y}_i)^2 \quad \dots(4)$$

$$STC = \sum_{i=1}^N (y_i - \bar{y})^2 \quad \dots(5)$$

SCR: Sum of squared residuals

Results and Discussion

Evolution of the Average Temperature

Figure 2 illustrates the average temperature changes in the digester throughout the experiment. The overall trends appear to be consistent. The average temperatures ranged from 23°C to 33°C, with a mean of 26.5°C ± 0.33. These mean temperatures fall within the mesophilic temperature range. However, they are lower than the optimal temperatures suggested by the researchers^{32,33} for cow dung's mesophilic digestion (29 and 35°C) and the researcher³⁴ for anaerobic co-digestion of pig slurry with bio-waste from pineapple peel in a continuously stirred reactor (37 ± 1 °C). Maximum temperatures close to these optimal ranges for the substrates (T, B, T+B, B+C) were only recorded on around 9 days out of the 45-day trial. This is comprehensible given that the tests were conducted during the rainy season and by the addition of extra water to the waste. Adding water to cow dung in a 1:2 ratio³⁵ found that this required a large amount of heat to keep the temperature high enough to allow bacterial activity. According to study,³⁶ the wastes

in the present study are being evaluated for their suitability for biogas production under sub-optimal conditions. Nevertheless, according to a number

of recent research, the mesophilic degradation temperature of agricultural waste should be between 21 to 40°C.^{37,38}

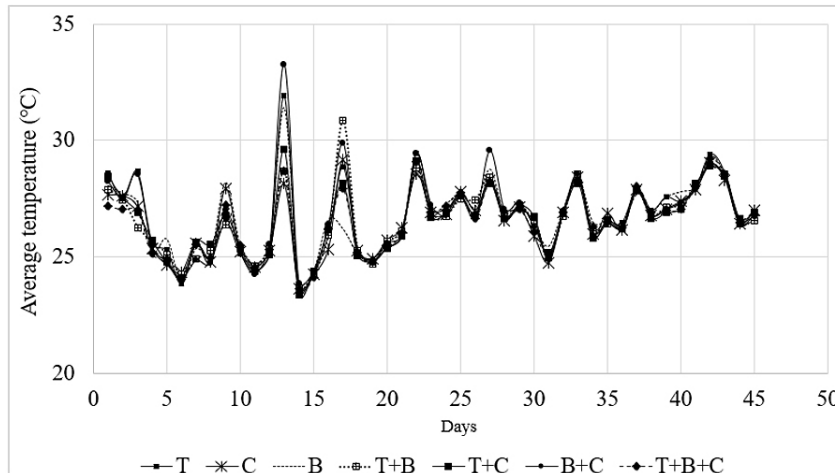


Fig. 2: Average temperature variation of the digestion (C: crown; T: Cake; B: cow dung)

Evolution of Average pH of Substrates

Figure 3 illustrates the evolution of average pH during the experimentation. The initial pH of substrates composed of cow dung (B) and the mixture of cow dung and crown (B+C) are close to neutral at 7.1 and 6.7 respectively. The acidic nature of the other substrates, especially the cakes + crowns (T+C), emphasizes the positive impact of blending vegetable and animal matter in specific proportions.

The trends observed during the experiment are similar for all the trials. There was a fluctuation in pH over the initial 3 weeks, resulting in a relative drop. This decrease in pH is attributable to the production of volatile fatty acid (VFA) by acid-generating bacteria at the initial stages of the process.

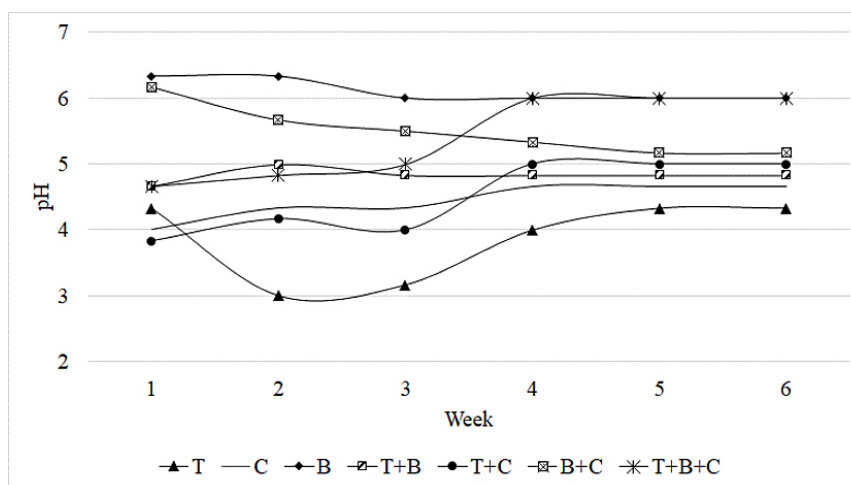


Fig. 3: Average pH variation of the substrate (C: crown; T: Cake; B: cow dung)

This trend in pH evolution is similar to that achieved by researchers.^{39,35} It was not until the 4th week that pH values became stable. This stability was not preceded by a substantial increase, as in the results obtained by researchers^{39,35} where pH increased to its normal operating value before stabilizing. According to these authors, the gradual increase in pH at the end of start-up appears when VFAs are consumed by methanogens and transferred to methane. Additionally, protein hydrolysis and amino acid production could also lead to an increase in pH. This was not observed in the present study.

Furthermore, the pH values of all substrates in the present study remained below the optimal pH range for methanogens (6.8-7.6). At pH values below 6.6, the growth of these bacteria is significantly reduced, resulting in suboptimal performance. This imbalance

and the low pH can be corrected by incorporating NaOH or HCl in the pre-treatment or during the fermentation period, as previously described by researchers.^{35,40} Similarly, researcher⁴¹ proposes that in the instance of an anaerobic digestion process run at low initial pH values of 4.5-5.5, buffers (e.g., $\text{H}_2\text{CO}_3/\text{HCO}_3^-/\text{CO}_3^{2-}$) and/or nutrients must be provided to make the alkalinity of the substrates higher to keep up neutral pH.

Evolution of Daily Biogas Production

Figure 4 shows the average daily biogas production. Biogas production started immediately from the 1st day of the experimental start-up date. This observation indicates that biogas production commenced at an early stage for all substrates, thus reducing the time required for startup.

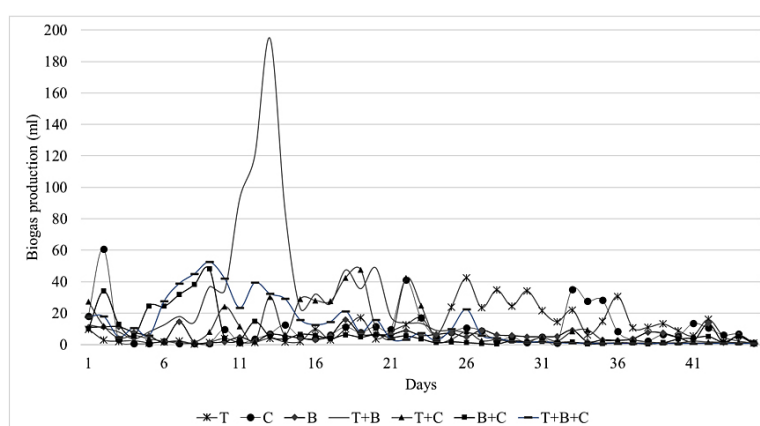


Fig. 4: Daily average biogas production (C: crown; T: Cake; B: cow dung)

This may be explained by the fact that microorganisms acclimated to the substrate during storage at the production site. These results are similar to those of researchers.^{33,42} After this start-up phase, daily biogas production fluctuated sharply. For substrate T, daily production ranged from 0.4 to 42.4 ml recorded on day 26th. For substrate C, production varied between 0.7 and 60.9 ml, with the highest levels recorded on days 2, 22, and 33. Substrate B produced very low daily yields ranging from 0.9 to 15.7ml (on the 18th day). Daily production of substrate T+B ranged from 1 to 194.7ml (obtained on the 13th day). For the T+C mix, high production levels were recorded on days 19 and 22, with

variations ranging from 1.3 to 47.6ml. For mixture B+C, values ranged from 0.4 to 48.1 ml (on day 10). The peak production period is between days 1 and 13.

For the T+B+C mixture, production varies between 0.7 and 52.6 ml (on day 9). These daily fluctuations can be attributed to three factors. Firstly, the variation in temperature for the trials.⁴³⁻⁴⁵ Study⁴⁶ showed that temperature spikes between 35°C and 30°C and between 30°C and 32°C were responsible for a decline in the output of biogas rates. However, no lasting damage to digestion performance was observed once temperatures had recovered. Secondly, they can be justified by the poor contact of

the substrate with the microorganisms, which limited the conversion of the substrate into biogas^{47,48} and thirdly, the acidity of the reaction medium induced a low pH. Single digestion of cow dung (B), cake (T) and crowns (C) shows the lowest daily biogas production compared to co-digestion. These results are similar to those of the study.⁴² Biogas production stabilized and almost ceased on day 28 for substrate T+B, and by day 35 for substrate T+B+C. For all other substrates, production continued, but very weakly, until day 45. This observation indicates that the residence times for these two substrates are shorter than those for the others. The cessation or

reduction in biogas production is linked to the lack of new nutrients. Anaerobic microorganisms process the substrate containing proteins and carbohydrates. As the quantity of these substances decreases, the biogas production process also slows down.⁴⁹

Cumulative Biogas Production

Each substrate's overall biogas production volume in the reactors is illustrated in Figure 5. This figure presents the sum of the daily biogas production over the 45-day experimental period. The volume produced in three replicates for each treatment was averaged daily.

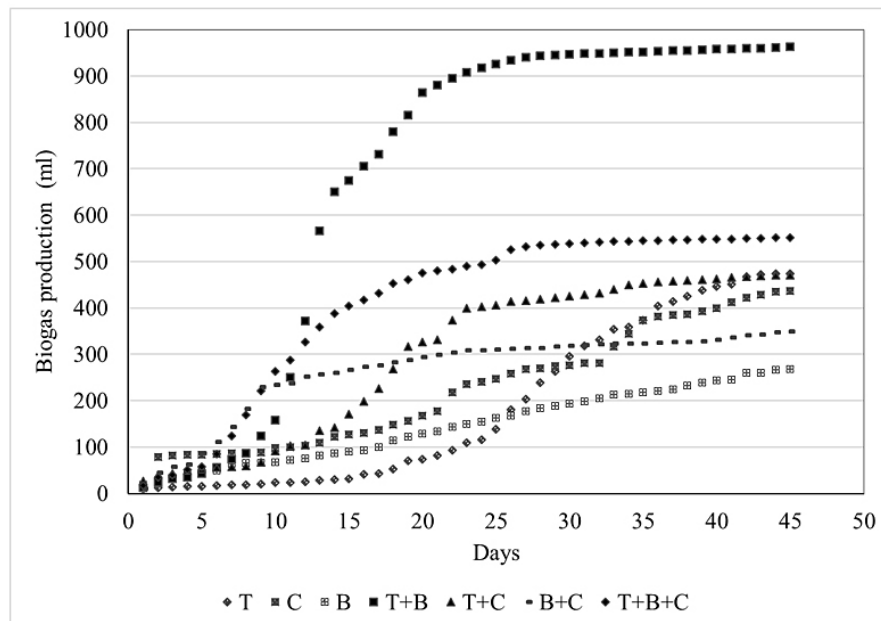


Fig. 5: Cumulative average biogas production (C: crown; T: Cake; B: cow dung)

The biogas production kinetics are ranked in the following order: (T+B) 883.033ml > (T+B+C) 599.063ml > (T) 467.11ml > (T+C) 425.675ml > (C) 384.241ml > (B+C) 311.975ml > (B) 259.71ml. The mixture of cakes with cow dung (T+B) yielded the highest biogas production. A comparison of this biogas production with that of the mixture of cake, cow dung, and crown (T+B+C) and the production of cake only (T) with that of cake and crown (T+C) indicates that the addition of the crown had an inhibitory effect on production. This is due to the slow degradation of this waste material, which is composed of a complex lignocellulosic structure, making it difficult for bacteria to digest the substrate.

From table 1 related to physico-chemical properties of substrates, % lignin > % hemicellulose > % cellulose in the crown. Inversely, % lignin < % hemicellulose < % cellulose in the cake. Study⁵⁰ highlighted the fact that the digestion of cellulose is superior to that of hemicellulose, which is also superior to that of lignin, while highlighting the fact that lignin is very difficult to digest. The efficiency of the process is limited during hydrolysis when microbial enzymes are unable to degrade the substrates.⁵¹

To optimize the digestion process of pineapple peels, researcher⁵² carried out a pre-treatment using

chemical agents such as sulphuric acid and alkaline hydrogen peroxide (H_2O_2) to solubilize the lignin in the matter. The use of a potassium hydroxide (KOH) solution has also been demonstrated to be effective.⁴⁰ The low biogas production of substrates T, T+C, C, and B+C in comparison to the other substrates (T+B and T+B+C) can be attributed to a great C/N ratio. Conversely, in the instance of cow dung (B), it can be justified by a low C/N ratio in comparison to the recommended optimum can be observed. A very great C/N ratio results in a nitrogen concentration that is insufficient for microbial growth⁵³ and an accumulation of unreacted carbon.⁵⁴

Conversely, a low C/N ratio, i.e. a high nitrogen content, leads to a build-up of nitrogen from ammonia and subsequent inhibition of the digestion process.^{53,55} Consequently, microorganisms need a C/N ratio that is suited to their metabolic processes.⁵⁶ For optimal biogas production, organic material must have a C/N ratio nearly 20-30. A C/N ratio of 30 has been found to result in biogas production that is 13.3-66.5% more than that with a C/N ratio of 25.⁴⁰ A study by researcher,⁵⁷ showed that nitrogen-rich supplements, such as swine manure and urea, corrected the imbalances caused by a high C/N ratio, highlighting the fact that urea is the best solution as it not only increases the nitrogen content of the digestate, but also promotes lignin degradation by speeding up the hydrolysis process.

It is challenging to make direct comparisons between the present results and the various biogas production curves found in the literature due to the differing experimental approaches employed, which result in data expressed in different units.⁵⁸ Table 3 compares the results obtained with cow dung with other studies at mesophilic temperatures.

Table 3: Comparison of the cow dung results with others studies at mesophilic temperature

	Quantity of biogas (liters/kg)	Test duration (day)
Present study	2.6	45
Study 59	15.6	25
Study 35	57.45	63
Study 60	0.38	41

The biogas production observed in this study with cow dung (2.6 liters/kg) is notably lower than that reported by study⁵⁹ (15.6 liters/kg). In the case of this study, the batch reactor is made of glass, whereas in study⁵⁹ study, the batch reactor is made of plastic. The reactor material can therefore also have an impact on the difference in biogas yield from cow dung through temperature variation. According to researcher,⁶¹ biogas production efficiency is influenced by substrate composition.

In particular, animal manure may contain inhibitory agents, including recalcitrant or toxic materials like ammonia (or its excess), sulfide, both light metal ions and heavy metals like Na, K, Mg, Ca, and Al.⁶²⁻⁶⁴ These compounds originate from commercial feeds or animal feed additives that encourage rapid growth and guard against cattle illnesses. No analysis of possibly hazardous or inhibiting substances was done in this study. Their compositions depend on the composition of their feed.^{49,65}

Nevertheless, the results indicate that all the substrates tested can be utilized for biogas production.

Biogas Production Predictive Model

The analysis of the mixing plan carried out in MINITAB has enabled us to propose a law that predicts biogas production as a function of the proportions of materials added. The linear model was selected to fit the experimental results and is presented by the following equation.

$$V_{\text{biogas}} = 481.4T + 275 B + 444 C + 2217 TB - 85 TC - 164 BC \quad \dots(6)$$

with $T+B+C = 1$

The value of the R^2 coefficient associated with the model estimate is 87.17%, and that of the adjusted R^2_{aj} coefficient is 82.9%. This indicates good predictive quality of the biogas potential. This predictive quality is confirmed by Figure 6, which illustrates the biogas potentials obtained by the relationship and their mean values measured experimentally. The fitted values overlap well with the mean experimental values.

The curves show increasing cumulative production from the 1st to the 28th day for substrates T+B,

T+B+C, T+C, B, and B+C. For the remainder of the digestion period, cumulative production tends to stabilize. For the total digestion time (45 days), biogas production kinetics are ranked in the following order: (T+B) 962.4ml > (T+B+C) 551.71ml > (T) 473.92ml > (T+C) 471.24ml > (C) 436.52ml > (B+C) 311.975ml > (B) 267.58ml.

The results of model validation by analysis of variance are presented in Table 3. Given that the value of p for T*B is less than 0.05%, we can deduce that production performance depends in particular on the proportions of cake and cow dung.

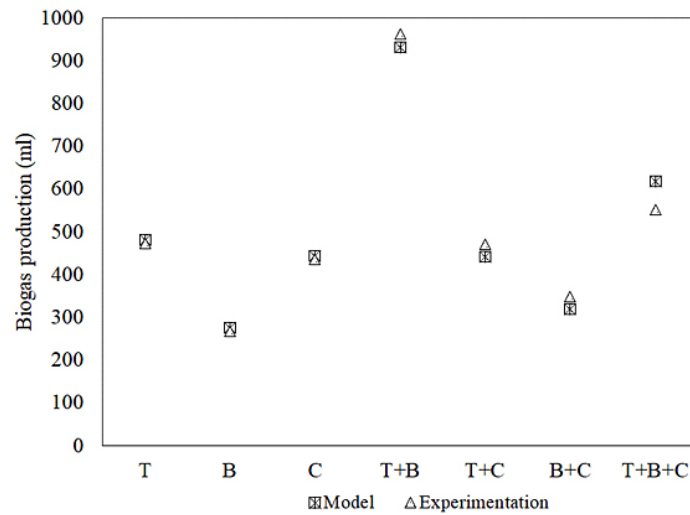


Fig. 6: Biogas potentials obtained by the predictive model and mean experimental values

Table 3: Variance analysis

Source	DL	SomCar seq	SomCar ajust	CM ajust	F Value	p-Value
Regression	5	874916	874916	174983	20.39	0.000
Linear	2	156932	72516	36258	4.23	0.035
Quadratic	3	717985	717985	239328	27.89	0.000
T*B	1	713287	703375	703375	81.97	0.000
T*C	1	863	1037	1037	0.12	0.733
B*C	1	3835	3835	3835	0.45	0.514
Residual error	15	128720	128720	8581		
Inadequate fit	1	22042	22042	22042	2.89	0.111
Pure error	14	106677	106677	7620		
Total	20	1003636				

Conclusion

This study evaluated the biogas production potential of pineapple waste (cakes and crowns) in mono and co-digestion with cow dung using different mixing ratios. The study was conducted at ambient

temperature, with a variation between 23 and 33°C. The results demonstrated that the cake-cow dung (T+B) and cake-dung-crown (T+B+C) mixtures exhibited the highest biogas production performance. It is noteworthy that the pH of the

various mixtures was not optimal for the digestion tests, as they remained below neutral throughout. It would therefore be beneficial to investigate the incorporation of buffers and/or nutrients into the substrates to enhance biogas production performance while keeping the reaction temperature stable. Tests combustion of biogas from each substrate also deserve to be done.

Acknowledgement

We would like to thank Promo Fruit Benin for collecting pineapple waste.

Funding Sources

The author(s) received no financial support for the research, authorship, and /or publication of this article.

Conflict of interest

The author(s) declares no conflict of interest.

Data Availability Statement

This statement does not apply to this article.

Ethics Statement

This research did not involve human participants, animal subjects, or any material that requires ethical approval.

Informed Consent Statement

This study did not involve human participants, and therefore, informed consent was not required.

Author Contributions

- **Djonoumawou Mèmèvègni Grâce Floriane Chidikofan:** Conceptualization, Analysis, Supervision, Writing – Review and Editing.
- **Thierry Gorlon Godjo:** Supervision and reading.
- **Josias Emen Ayao Dossa:** Conceptualization, Methodology, Data Collection, Analysis, and Writing – Original Draft.
- **David Gildas Farid Adamon, Melhyas Kplé and Guevara Nonviho:** Manuscript reading and approval.

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